

# Pinch-off and Coalescence in Liquid/Liquid Mixtures with Surface Tension

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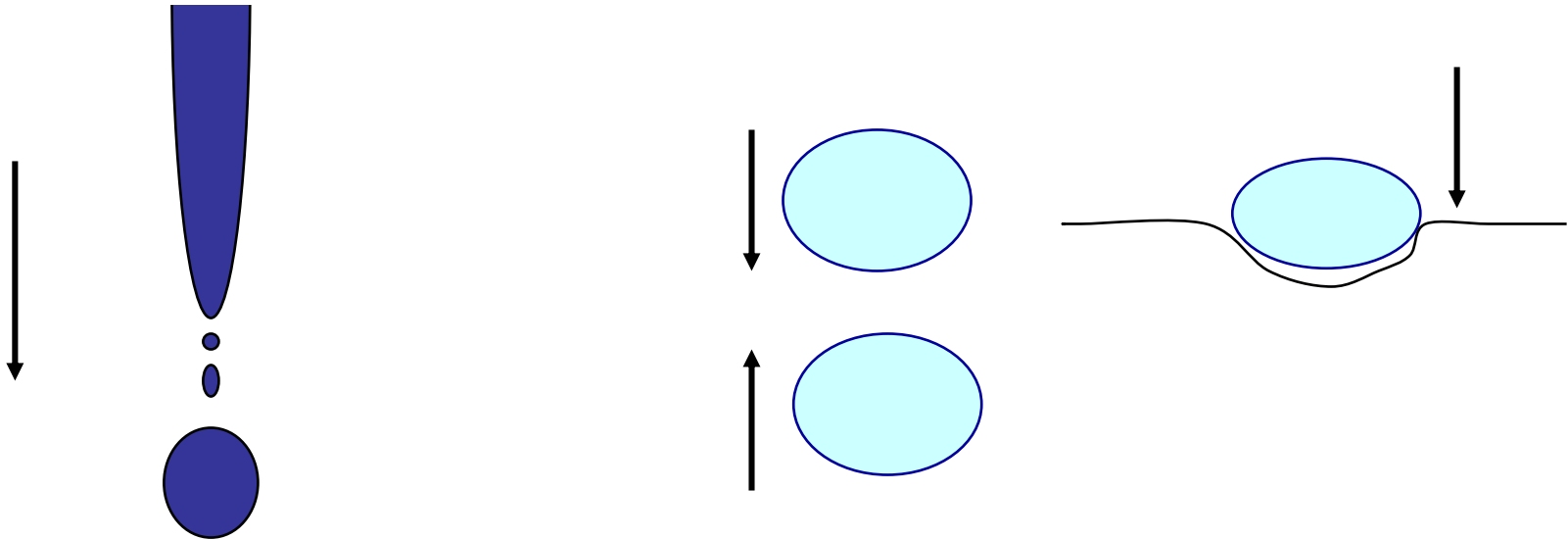
*University of Minnesota*

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# Motivation:

Develop accurate engineering-level models for transitions in multi-fluid flows with surface tension



Molecules at the interfaces must rearrange.

## Difficulties:

Transitions difficult to observe and model !

# Applications:

Transport, mixing, and separation of petroleum, chemical, food, and waste products



Issues: complex flow geometries  
large range of scales  
transition details affect process!

## Previous Work (pinch off):

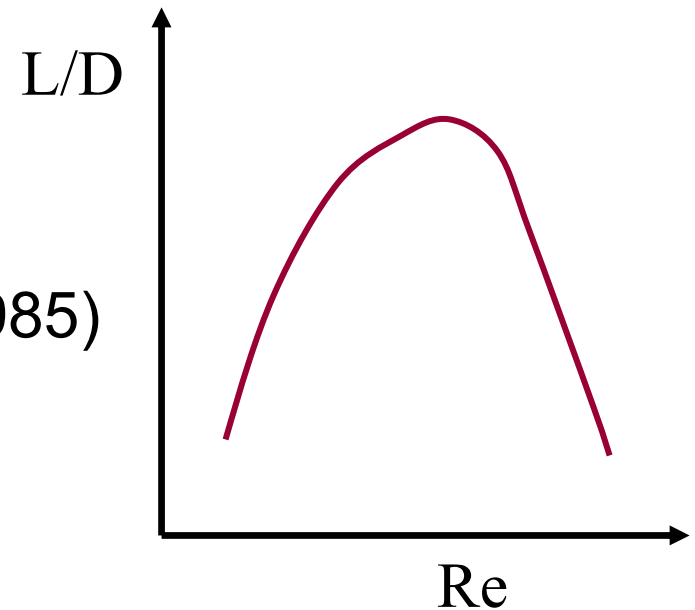
### Jets:

Scheele and co-workers (1969-1985)

Skelland and Johnson (1974)

Kitamura et al (1982)

Tadrust et al (1991)



Determination of instability modes, jet length before pinch off

### Straining and Dripping Flows:

Tjahjadi, Stone, Ottino (1992)

Cohen et al. (1999, 2001)

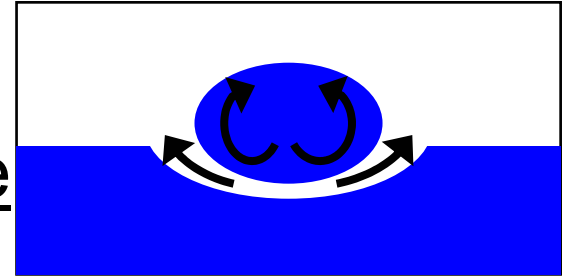
Zhang and Lister (1999)

Does flow become 'self similar' near pinch off locations?

# Previous Work:

## Drop coalescence at an interface

Hartland and co-workers (1967)



film shape and drainage rate, rupture characteristics,  $Re \ll 1$

Chi & Leal (1989), Manga & Stone (1995)

boundary integral methods, axisymmetric flow

## Drop/drop coalescence:

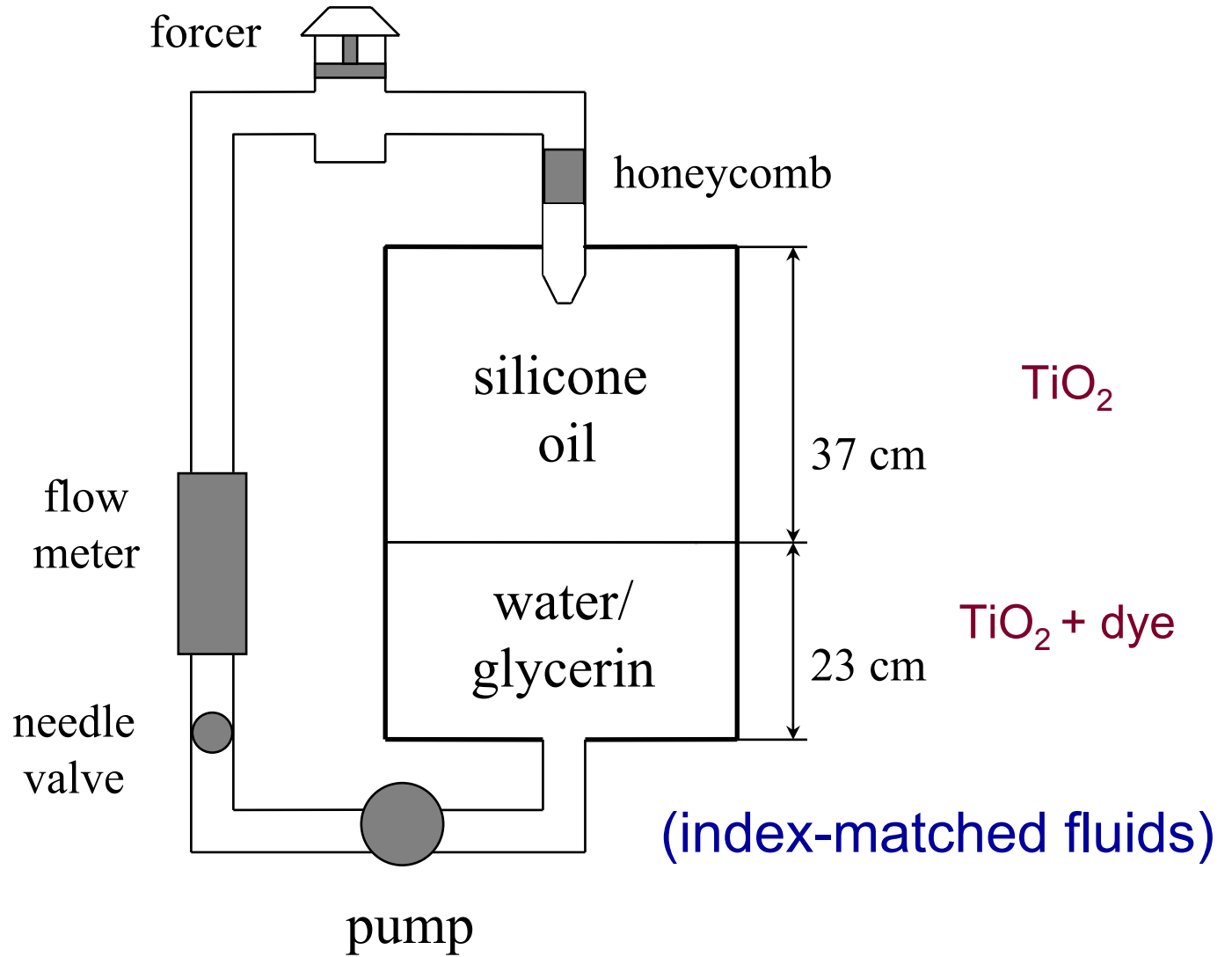
Leal and co-workers (2000, 2001, 2003)

Experiments in shearing flows at  $Re, We \ll 1$

# Objectives:

- Quantify transition dynamics in fundamental flows with significant inertia
- Compare with computations that include transition models
- Develop ‘physically-justified’ reconnection conditions for engineering-level codes

# Jet Facility



# Flow Parameters:

Glycerin/Water (50% by volume):  $\mu_i = 8.3 \text{ cp}$ ,  $\rho_i = 1.14 \text{ g/cc}$

Silicone Oil (Dow Corning 200):  $\mu_o = 4.8 \text{ cp}$ ,  $\rho_o = 0.96 \text{ g/cc}$

$D = 1 \text{ cm}$ ,  $\sigma = 0.0296 \text{ N/m}$

$$Bo = \frac{\Delta\rho \cdot g \cdot D_e^2}{\sigma} = 7.3$$

$$Oh = \frac{\mu_i}{\sqrt{\rho_i \cdot D_e \cdot \sigma}} = 0.015$$

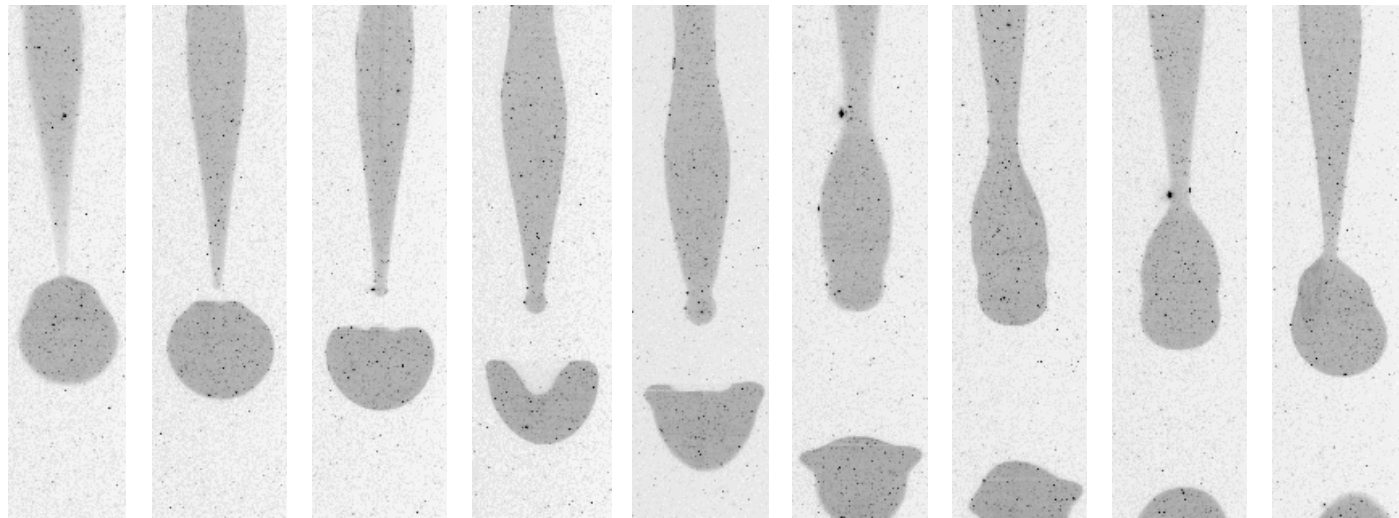
$$\lambda = \frac{\mu_i}{\mu_o} = 1.6$$

$$Re = \frac{\rho_i \cdot U_e \cdot D_e}{\mu_i} = 35 - 70$$

$$St = \frac{f \cdot D_e}{U_e} = 1.4 - 5.2$$

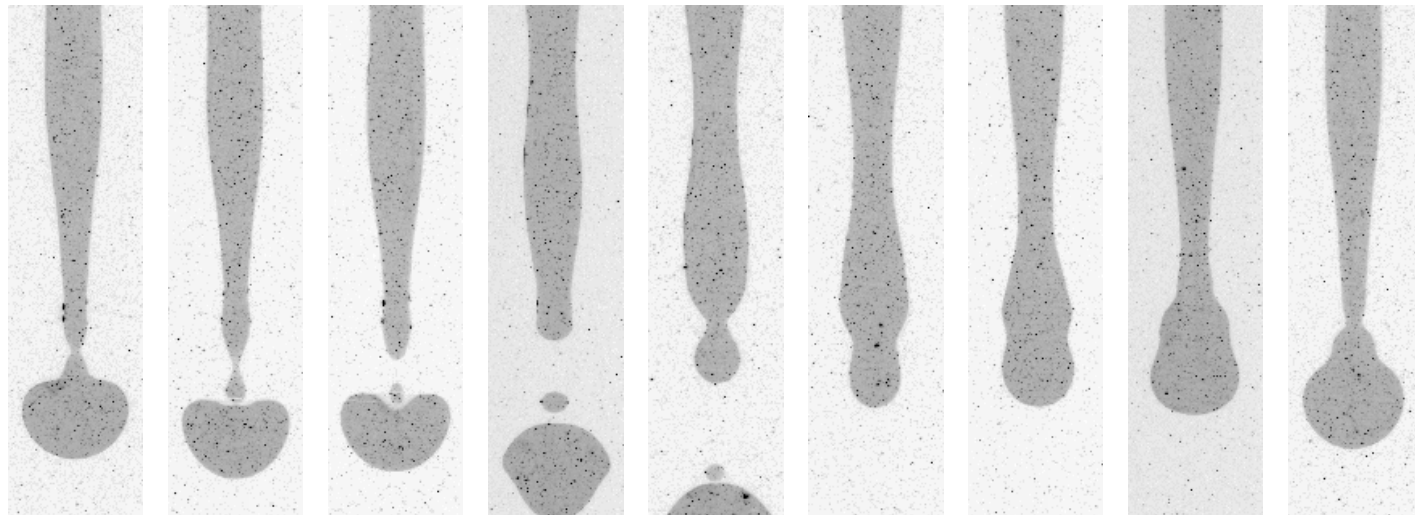


# LIF of Phase-locked flow: $St = 3.5$ , $\lambda = 1.6$



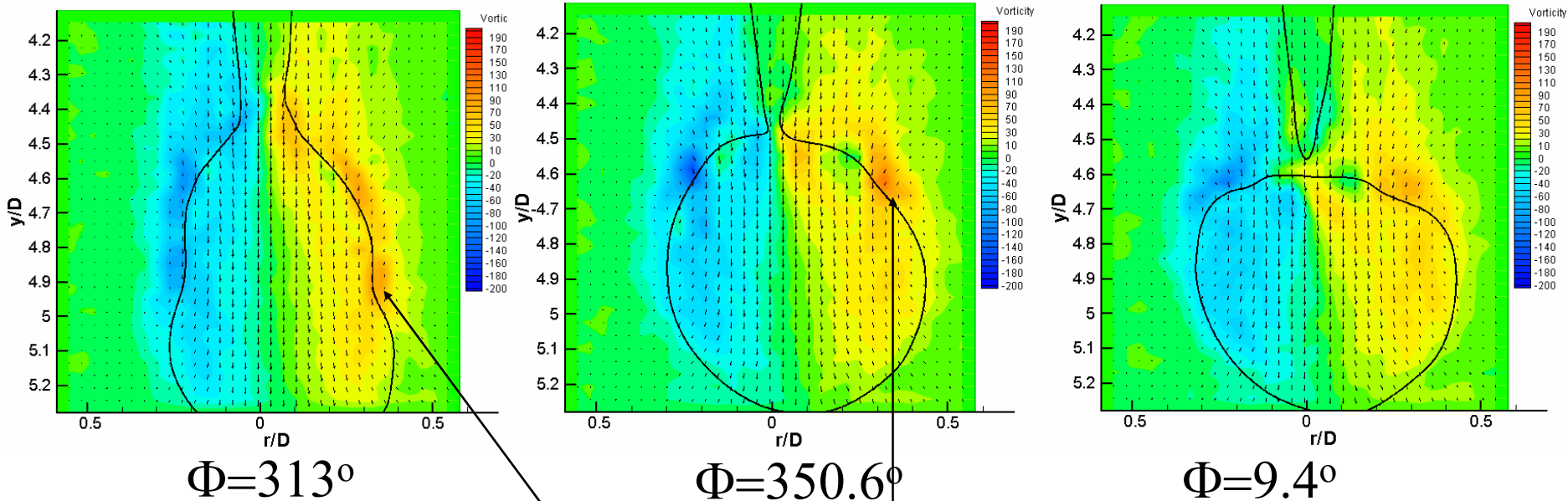
$Re = 58$

$0^\circ$     $20^\circ$     $40^\circ$     $100^\circ$     $160^\circ$     $220^\circ$     $260^\circ$     $300^\circ$     $340^\circ$



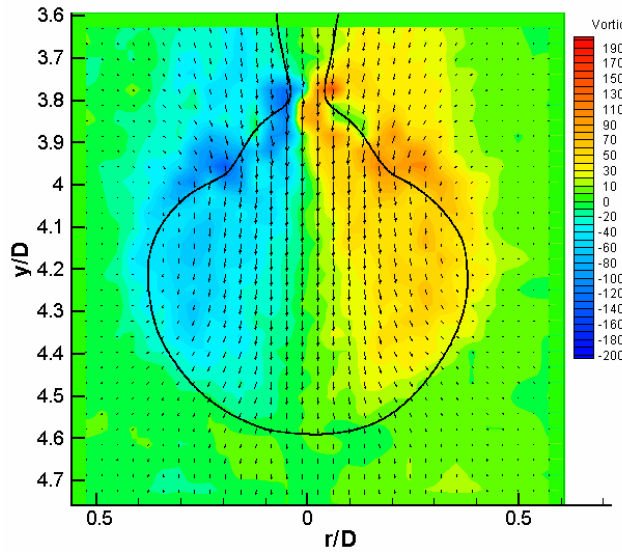
$Re = 39$

# Vorticity Contours: $Re = 58$ , $St = 3.5$

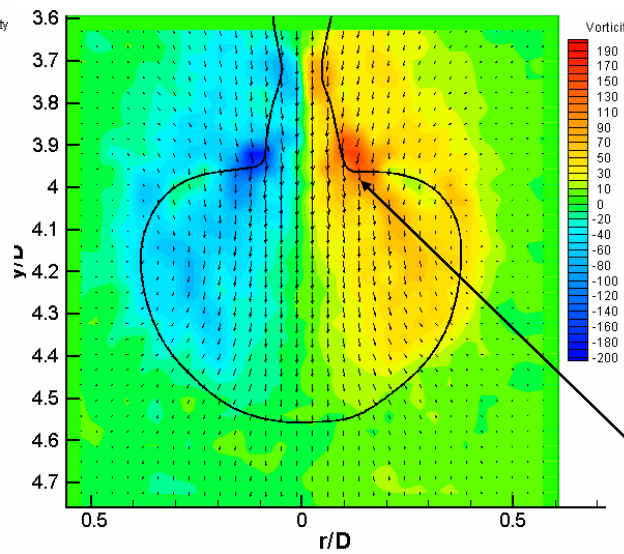


vorticity away from neck: no satellite

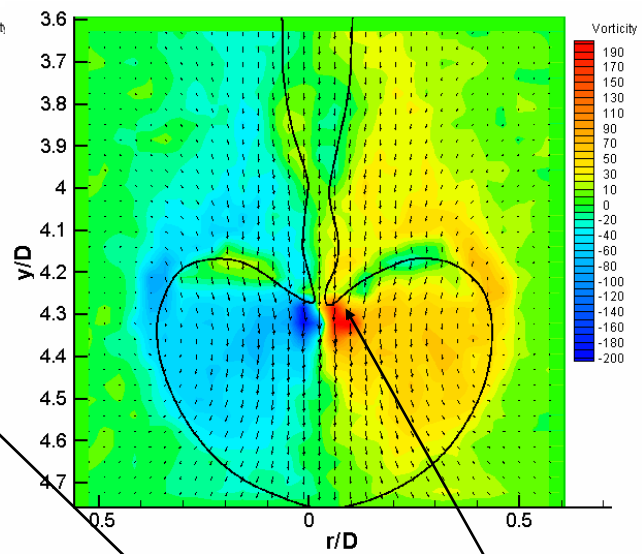
# Vorticity Contours: $Re = 39$ , $St = 3.5$



$\Phi = 327.5^\circ$

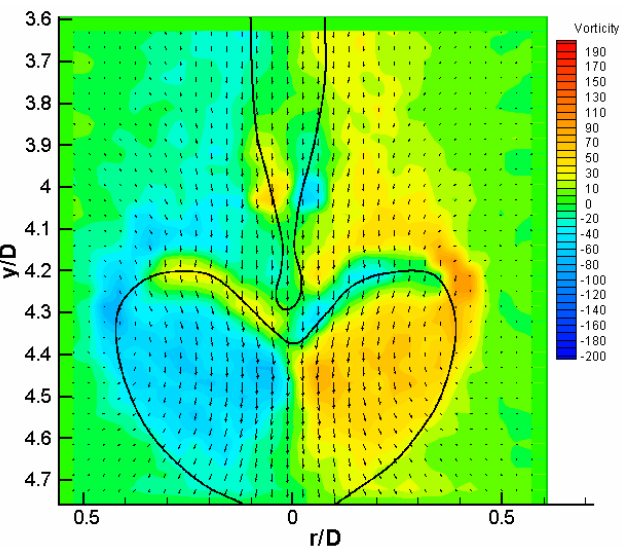


$\Phi = 340.5^\circ$

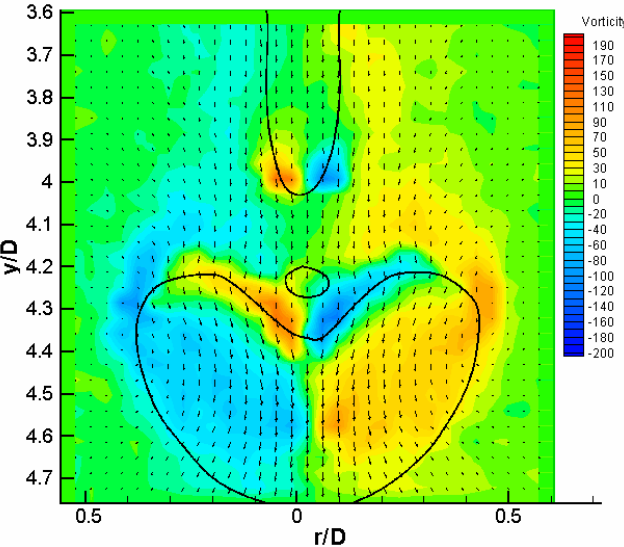


$\Phi = 353.5^\circ$

vorticity close to neck yields satellite

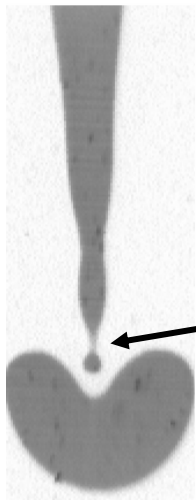


$\Phi = 6.5^\circ$



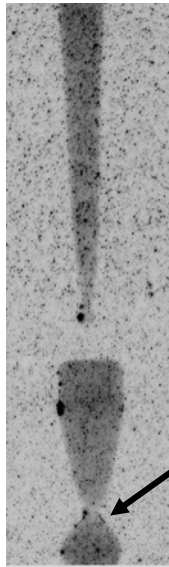
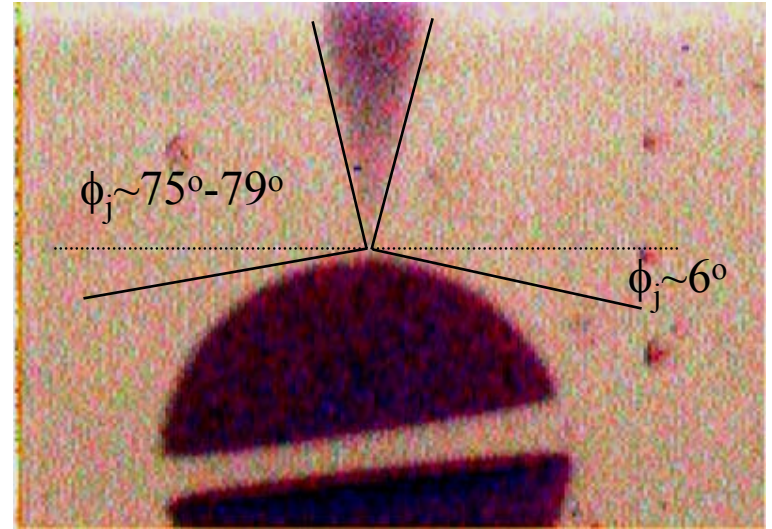
$\Phi = 13^\circ$

# Close-ups of pinch-off modes, $\lambda = 1.6$



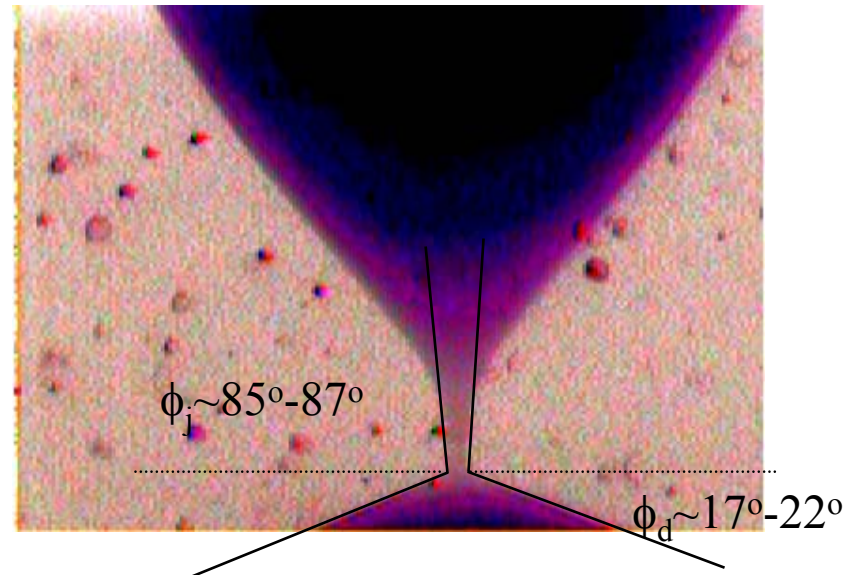
$Re = 39$   
 $St = 3.5$

jet/drop break



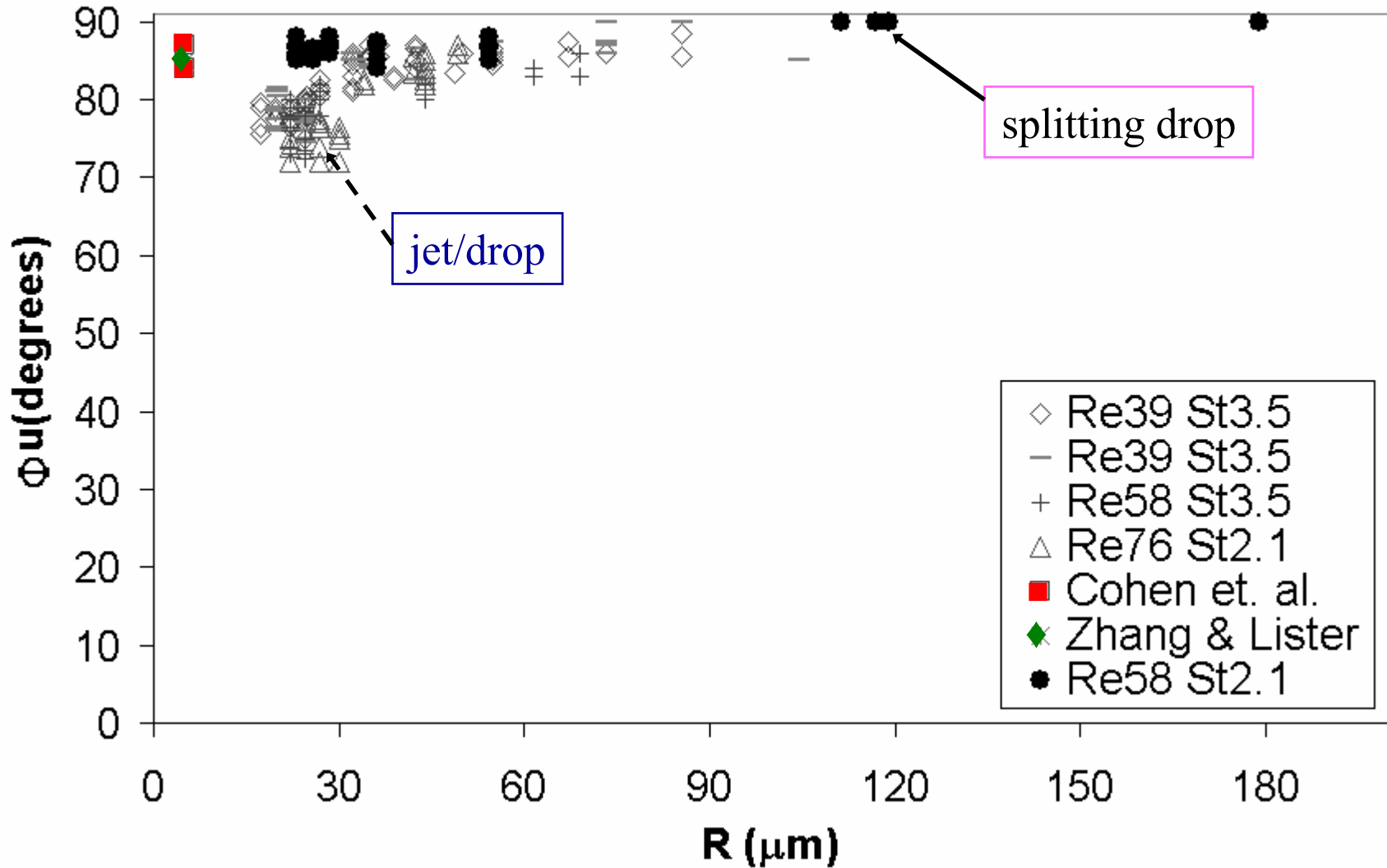
$Re = 58$   
 $St = 2.1$

splitting drop

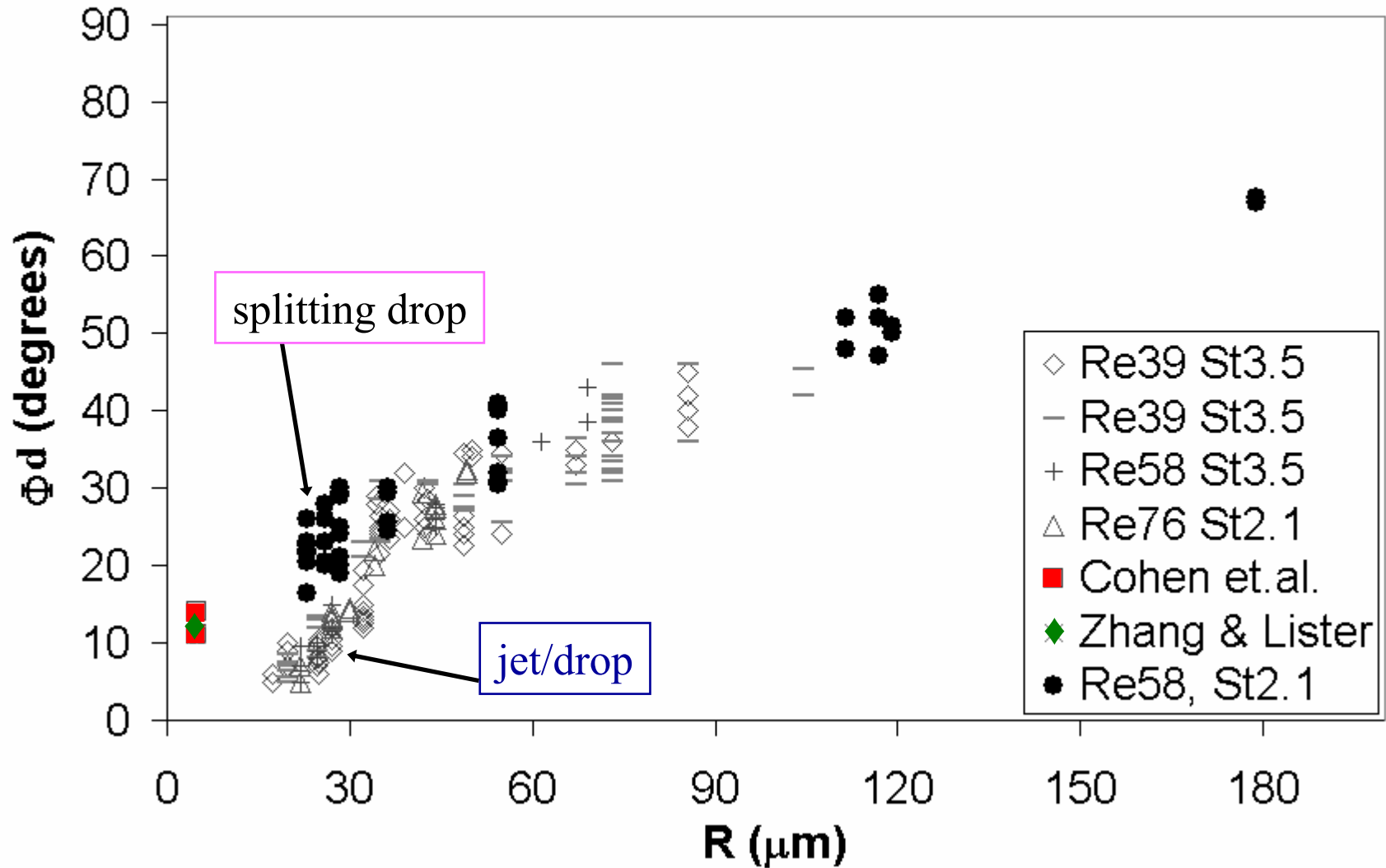


Do angles depend on  $\lambda$  only?

# Upper pinch-off angles



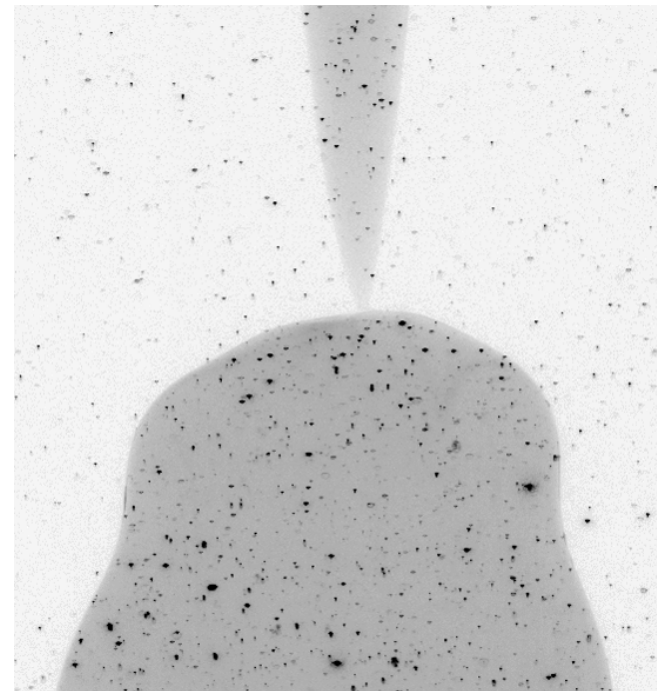
# Lower pinch-off angles



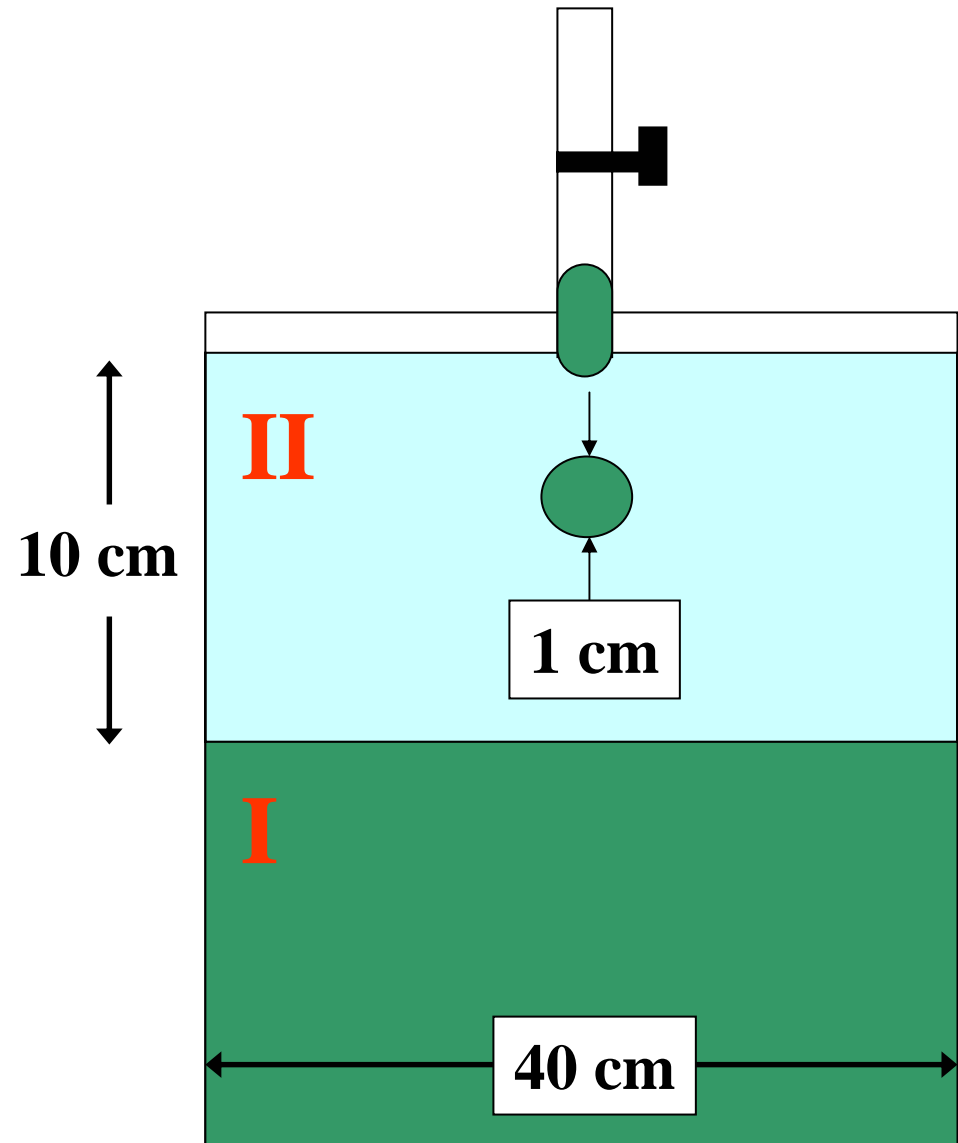
# Similarity Question:

- For scales  $\sim 15 \mu\text{m}$ :  
splitting drop mode converges toward similarity values  
jet/drop modes do not
- Stokes scaling valid for neck  $< 5 \mu\text{m}$

Does flow ever reach  
Stokes scaling??



# Coalescence Facility



II Silicone oil (50 & 5 cs)

I Water/glycerin mixture

$$\frac{\rho_I}{\rho_{II}} = 1.18$$

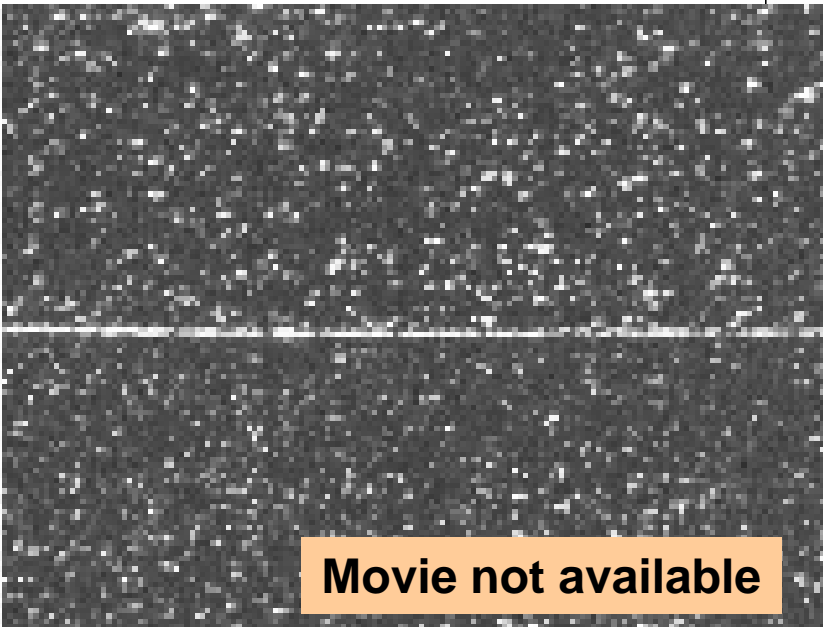
$$\lambda = \frac{\mu_I}{\mu_{II}} = 0.14, 0.33, 1.8$$

PIV image sequences  
acquired at 500 Hz



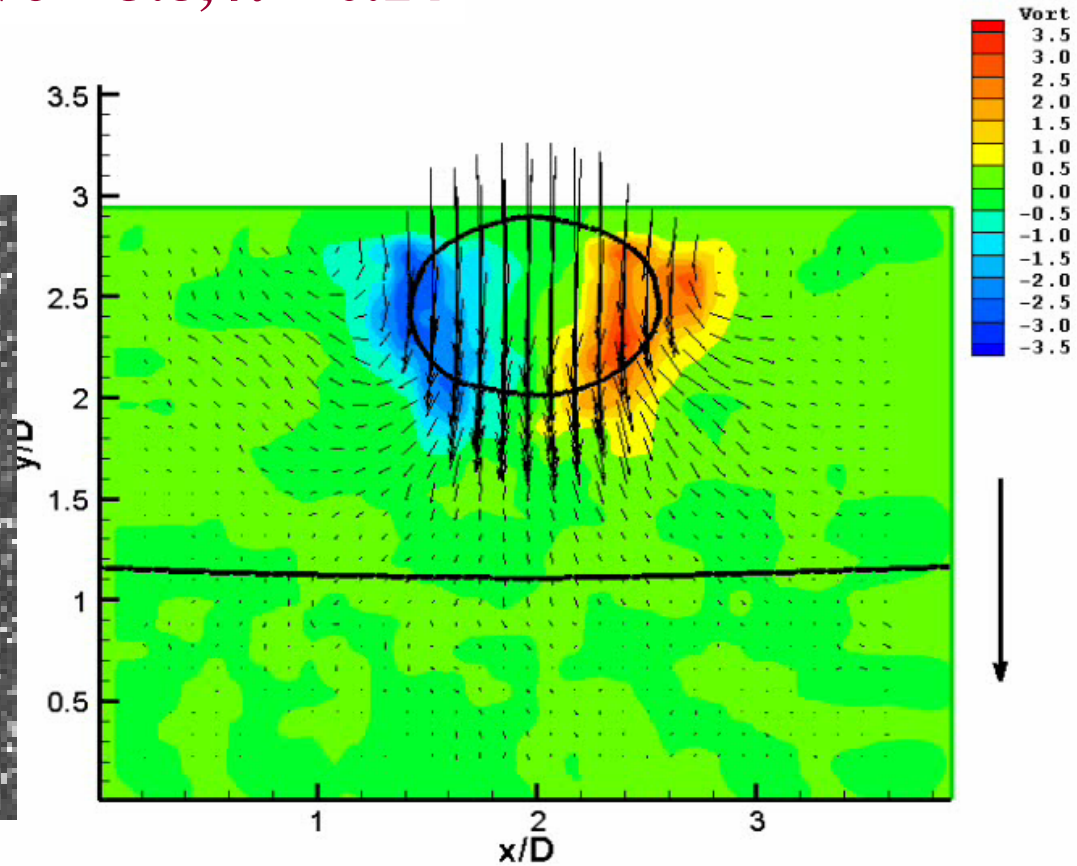
# Drop Impact

$Re = 20$ ,  $We = 3.8$ ,  $\lambda = 0.14$



Movie not available

1/30 of real speed



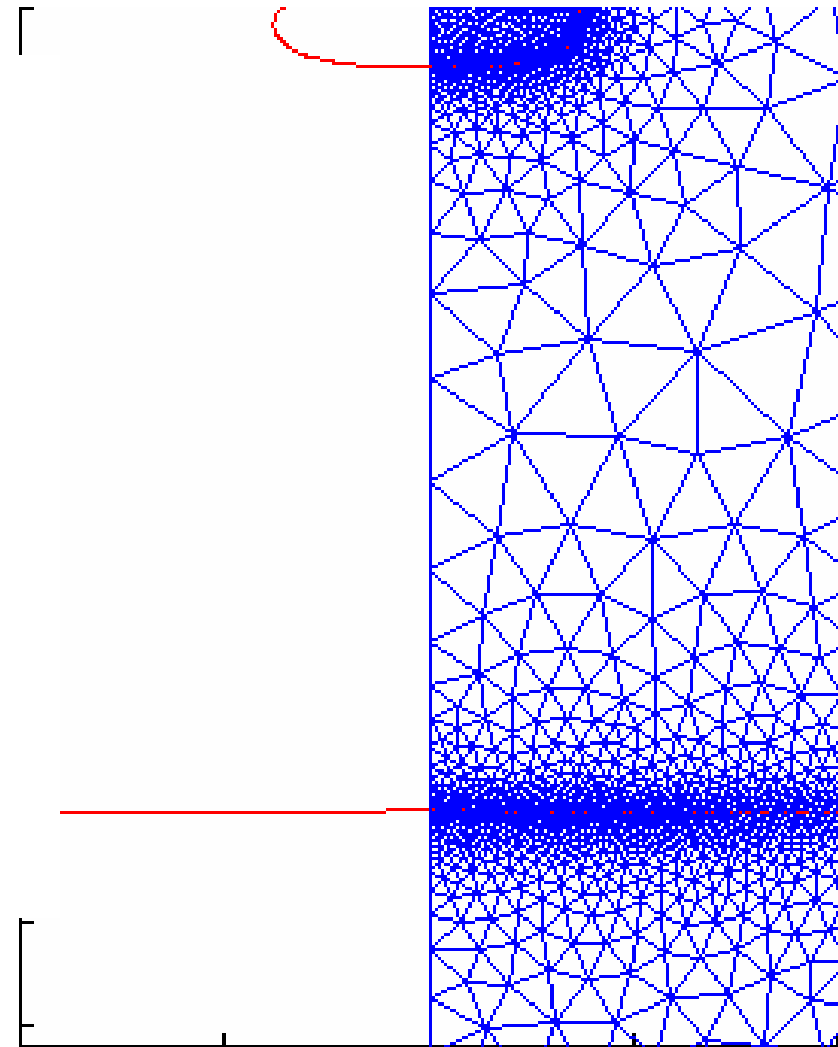
# Axisymmetric Simulation, Adaptive Grid

Finite Element Projection Method

Interface modeled as level set

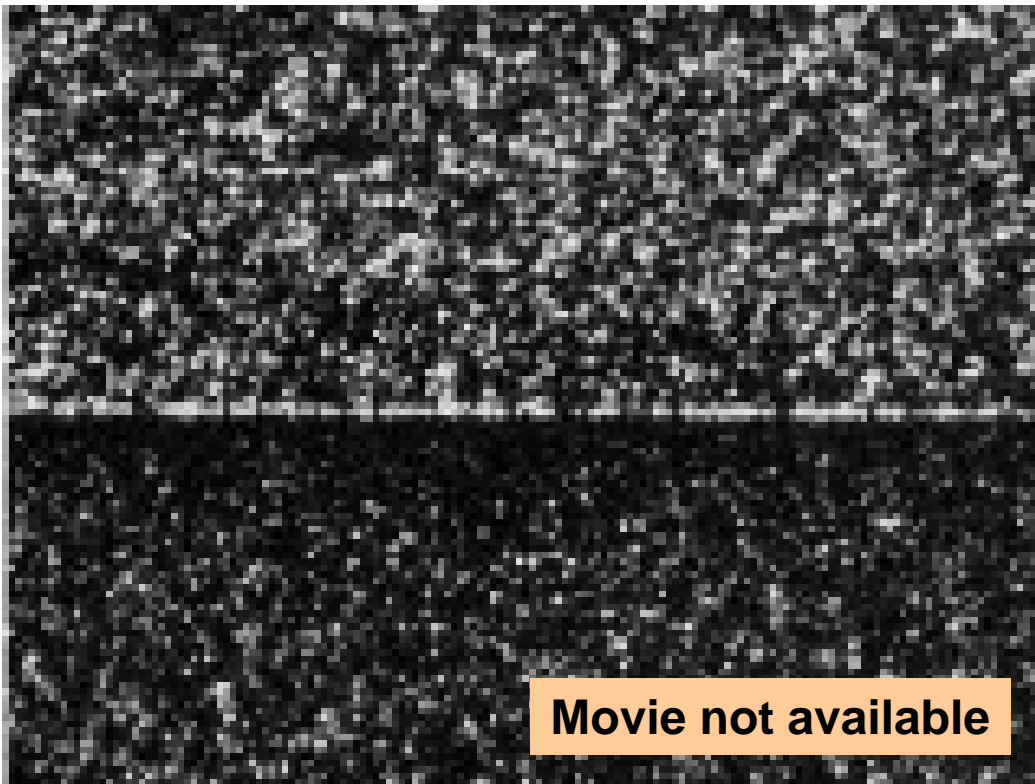
Surface tension is continuum surface force in momentum equation

Mesh size scales with distance from interface

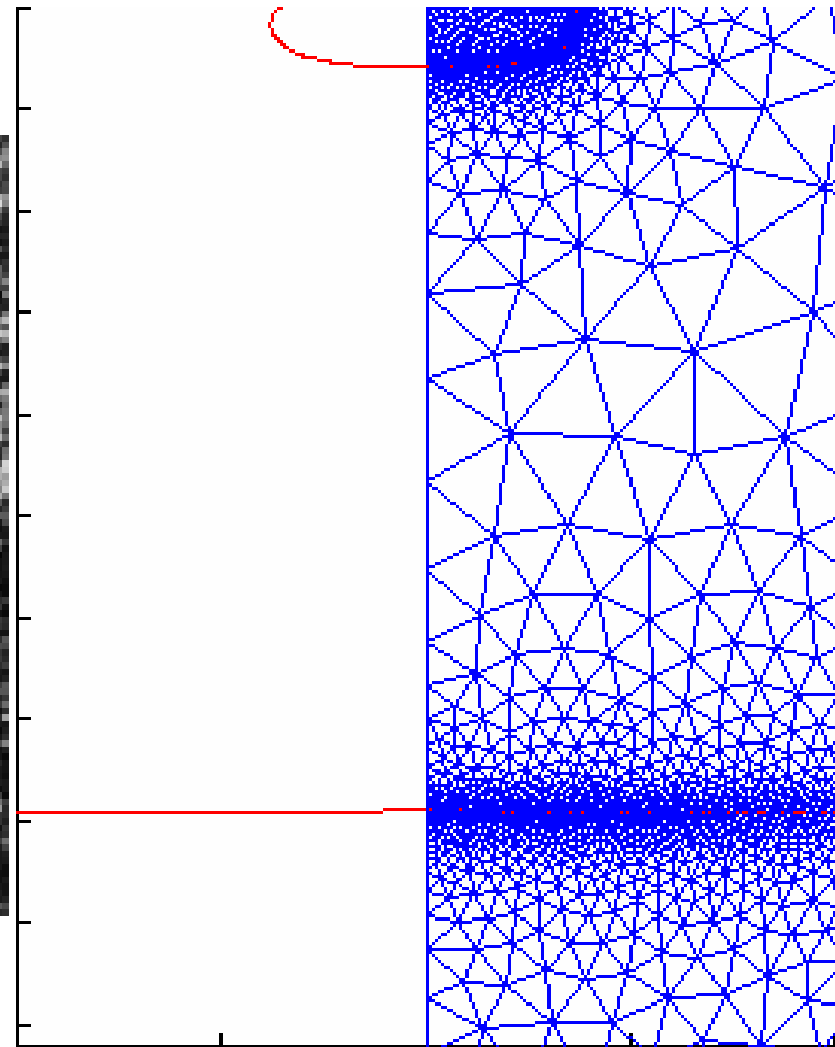


Zheng, Lowengrub, Cristini  
Talk NB4 on Tuesday

# Axisymmetric Simulation, Adaptive Grid

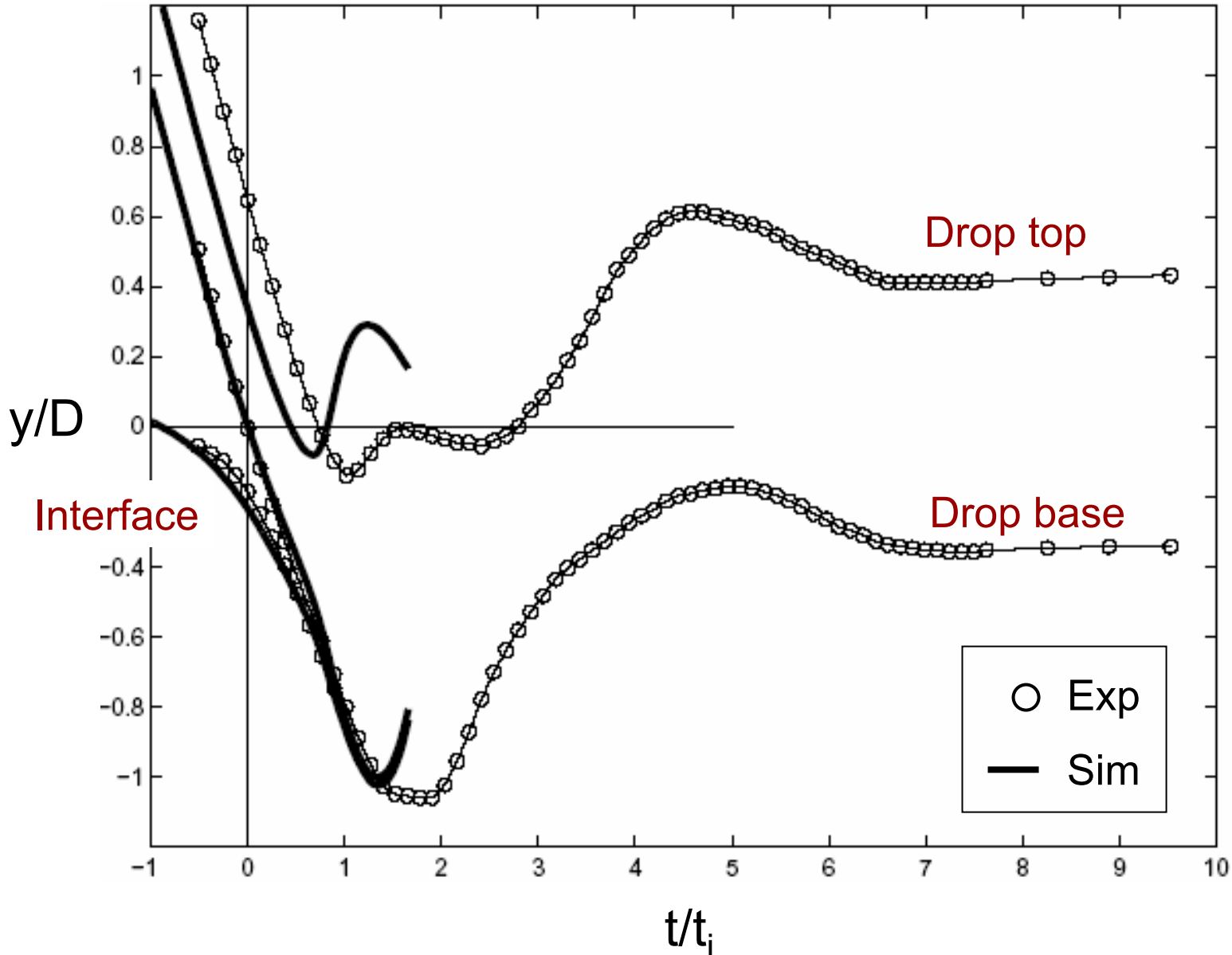


**Re = 68, We = 7,  $\lambda = 0.33$**

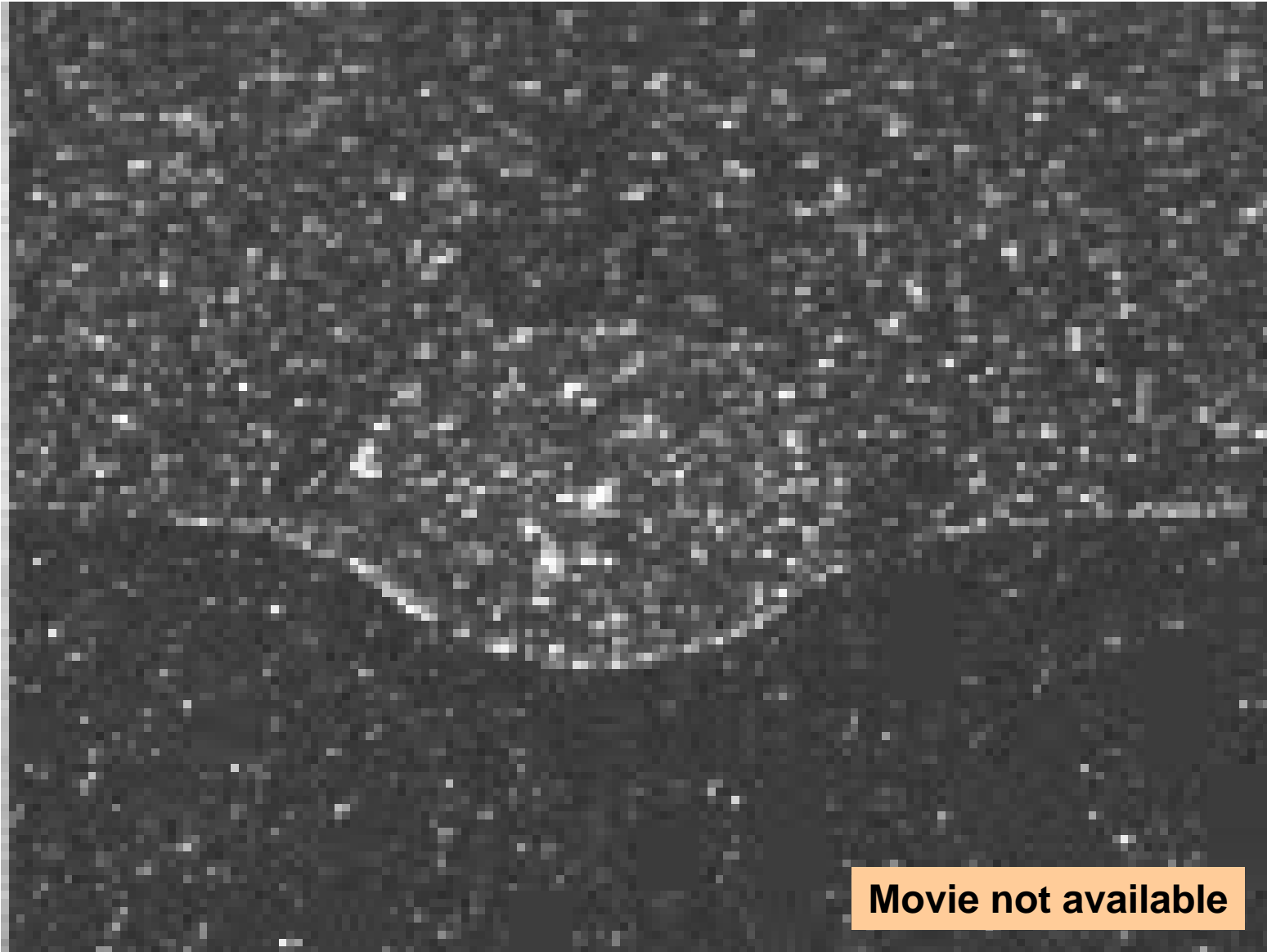


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# Vertical Interface Locations on Drop Axis



# Drop Coalescence

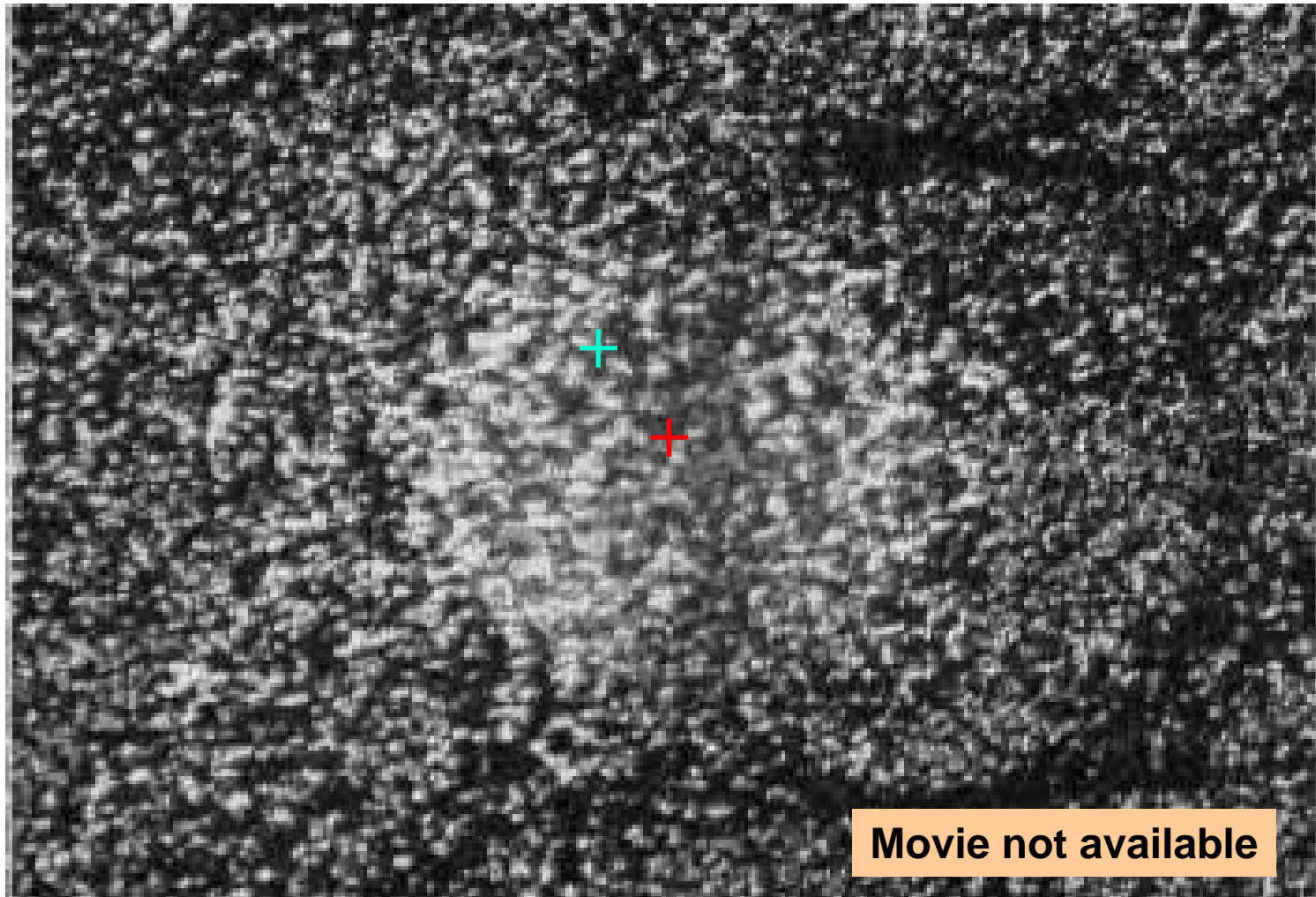


$\lambda = 0.14$   
 $Ca = 0.09$   
 $Bo = 6$

1/30 of  
real  
speed

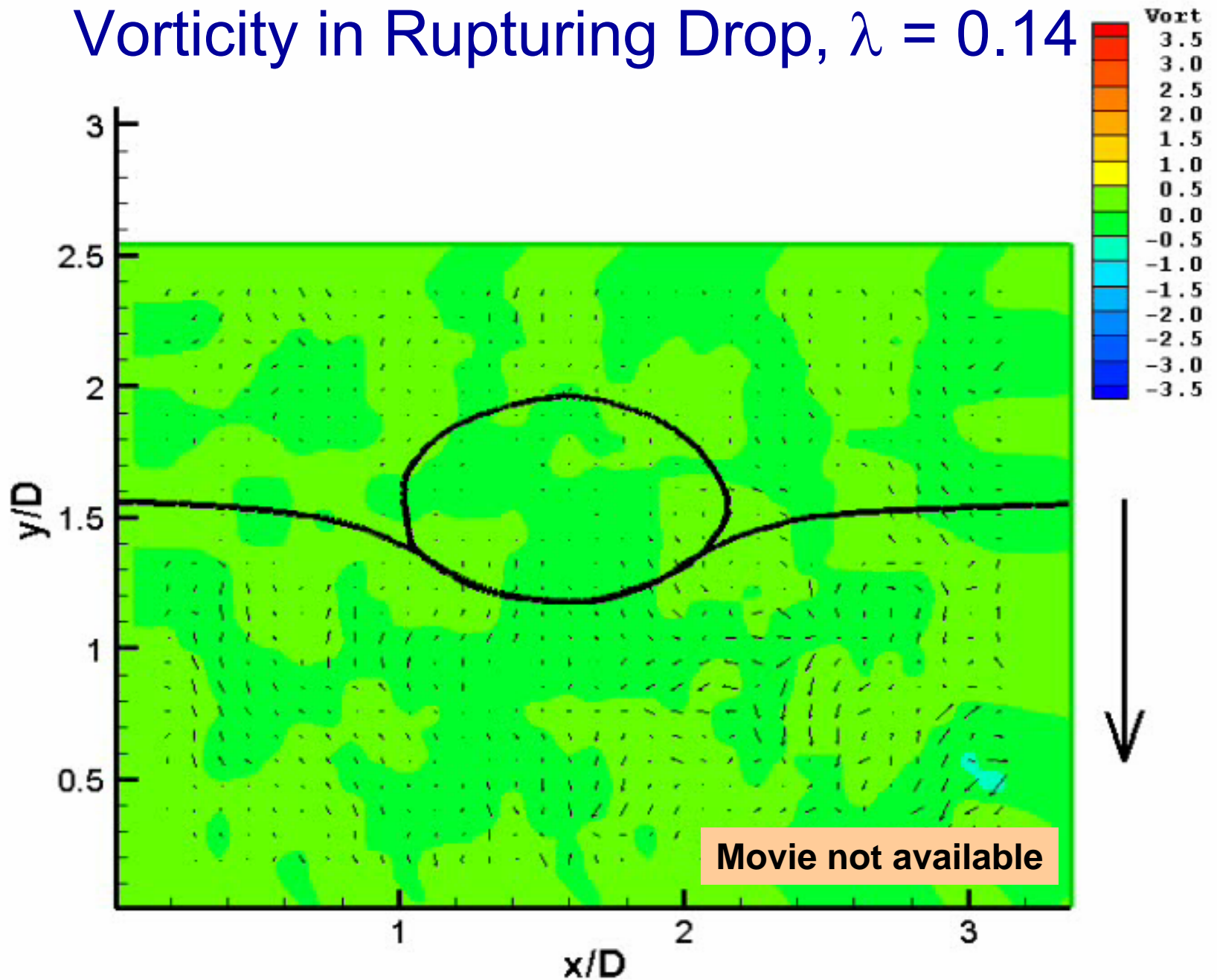
Movie not available

# Interface Rupture (horizontal plane)

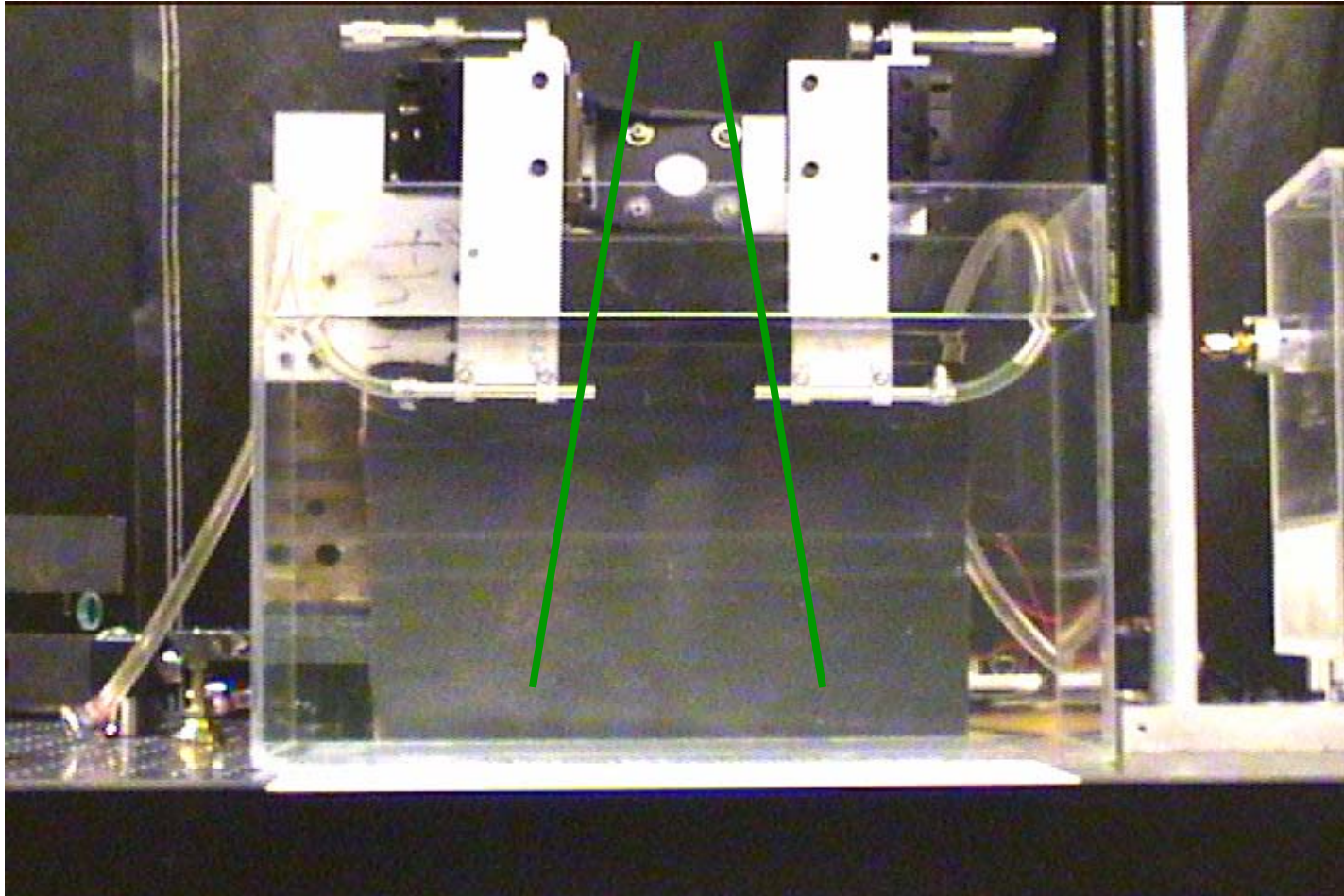


**+** = rupture point      **+** = drop centerline

# Vorticity in Rupturing Drop, $\lambda = 0.14$



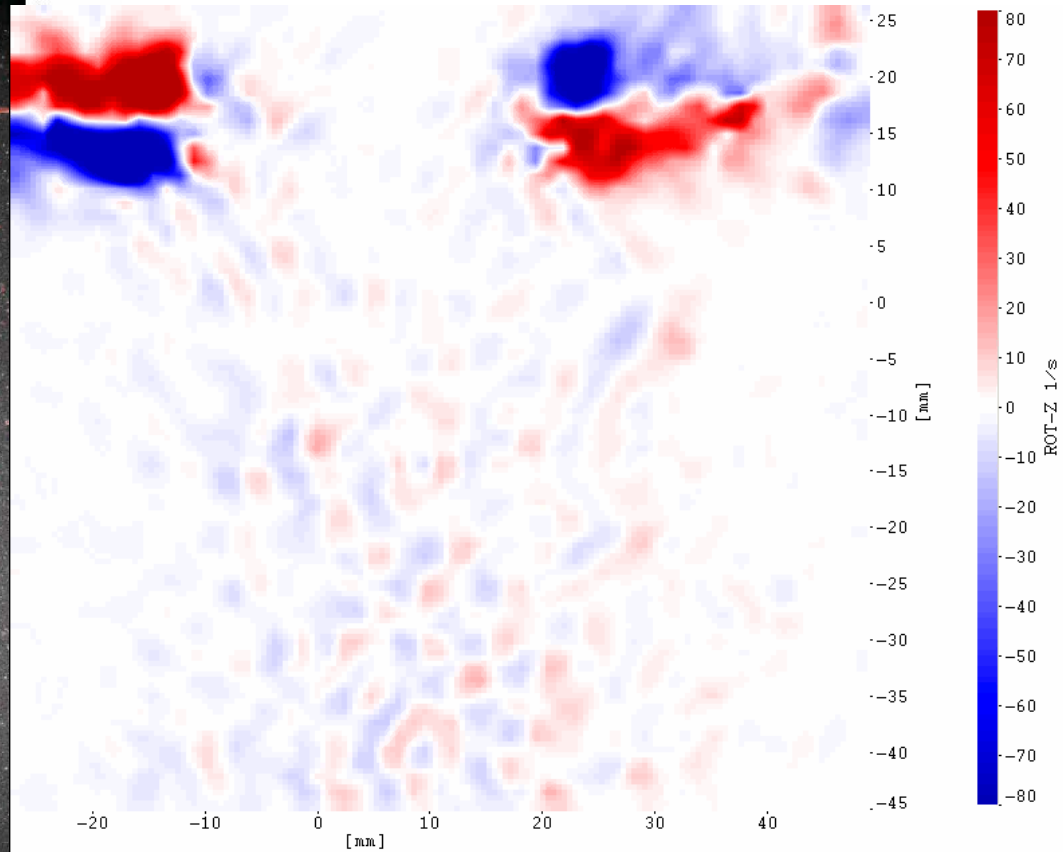
# Colliding Drop Pairs



High speed stereo PIV

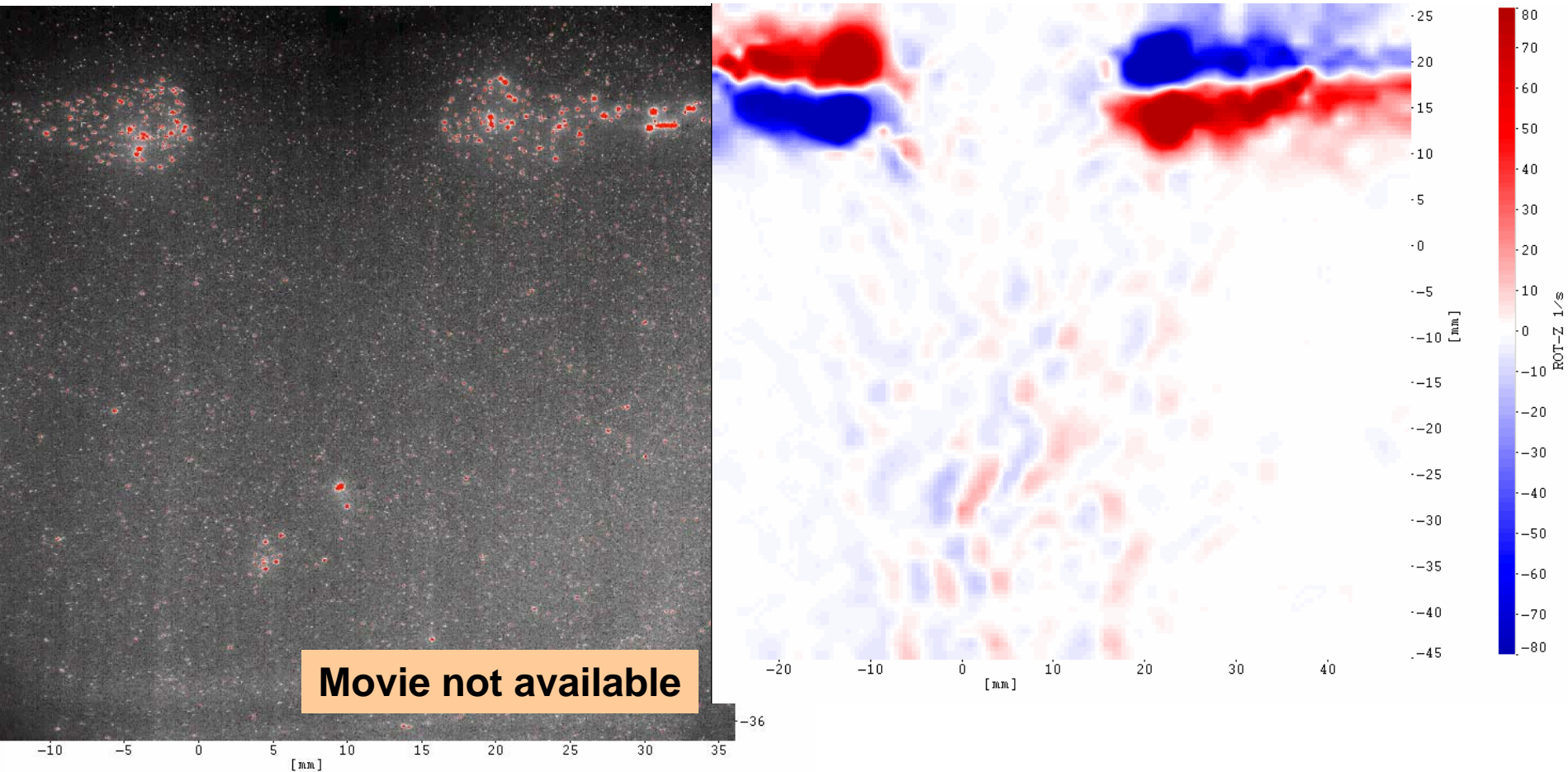


# Rebounding Drops



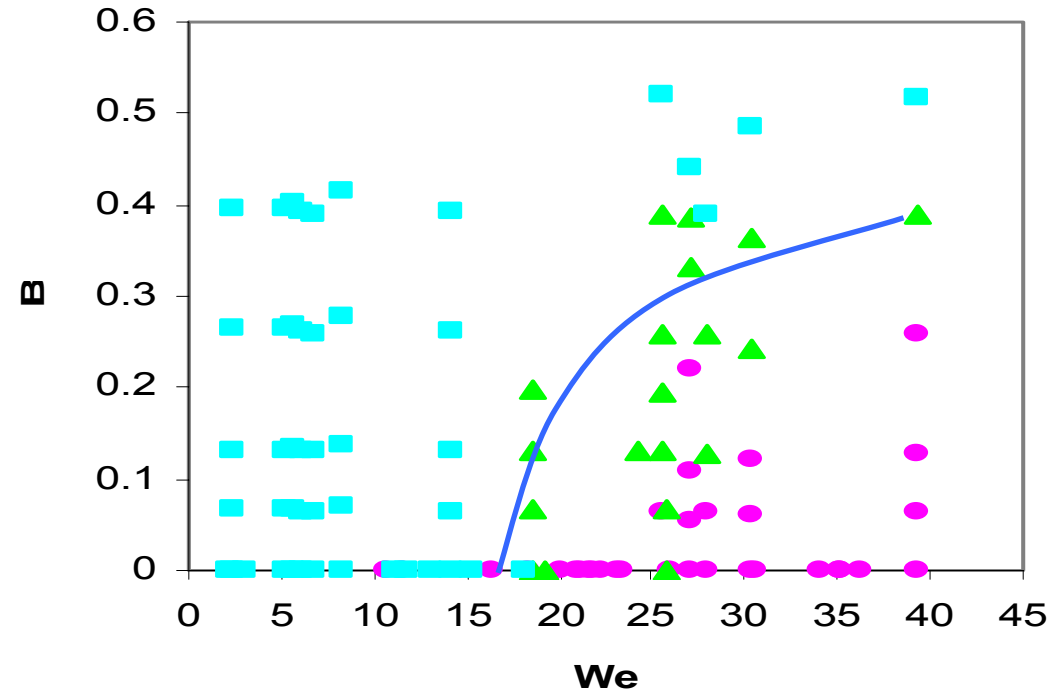
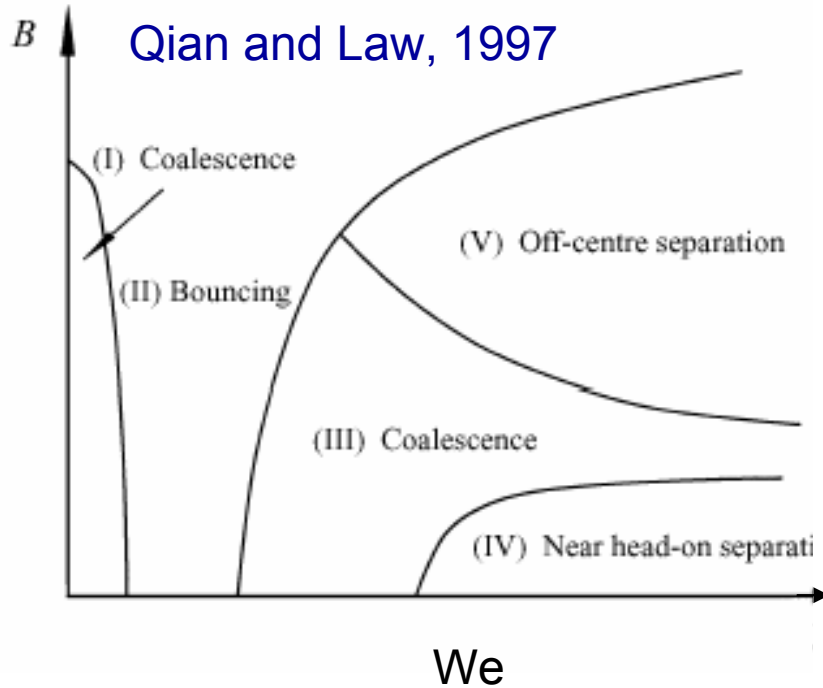
$$\text{Re} = 16, \text{We} = 4.5, \lambda = 0.14$$

# Coalescing Drops



$$\text{Re} = 29, \text{We} = 17, \lambda = 0.14$$

# Comparison to Drop Collisions in Gases



- Rebound/coalescence boundary has similar  $We$  for drops in gases and liquids
- ‘Separation’ at higher  $We$  also observed for drops in liquid

# Conclusions

## **Jet:**

Satellite formation encouraged by lower Re, outer viscosity  
Pinch-off angles not always consistent with similarity theory ?

## **Drop/Interface:**

Impact decoupled from coalescence:

$$0.3 < Re < 300 \quad (0.001 < Ca < 1)$$

Drop vortex dissipates during and after impact

Coalescence occurs off axis yielding 3D flow

Small scale behavior initiates large scale behavior

## **Drop/Drop:**

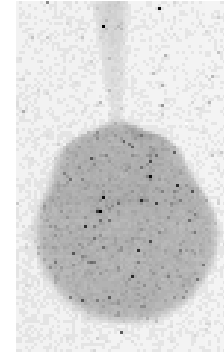
trends consistent with drop collisions in gases

including We at rebounding-coalescence boundary

# Future Work

## **Jet:**

Resolve jet neck to  $\sim 2$  micron to answer similarity question



## **Drops:**

Find parametric effects on coalescence time/topology

Resolve larger and smaller scales simultaneously to examine behavior near thin films

